



# **AUTOMATIC PUMP TRAP APST**

#### DESCRIPTION

The ADCAMat APST automatic pump trap is especially recommended where stall condition may occur due to poor steam trap condensate discharge capacity, caused by temporary insufficient pressure drop.

The equipment combines the features of a float steam trap and a pressure operated pump, in one single unit.

Whenever the steam trap function is incapable of draining condensate, the pump function is activated (using external steam pressure). The pump replaces the necessary positive pressure to lift the condensate to the return system, before water logging occurs, avoiding water hammer and consequent noise, equipment damage, corrosion, unstable temperature control, etc.



## MAIN FEATURES

High capacity.

Hardened stainless steel wear parts. High-endurance inconel springs.

Low filling head to minimize installation space.

No electric requirements or NPSH issues.

Suitable for hazardous environments.

Low running costs.

No motive or flash steam is lost. Operation under vacuum conditions.

OPTIONS: Level gauge.

USE: Drain and lift steam condensate from heat

exchangers, among others.

**AVAILABLE** 

MODELS: APSTS - carbon steel.

APSTS-HC – carbon steel, high capacity.

APSTSS - stainless steel.

APSTSS-HC - stainless steel, high capacity.

SIZES: 2" x 2" and 3" x 2".

DN 50 x 50 and DN 80 x 50.

CONNECTIONS: Flanged EN 1092-1 PN 16.

Flanged ASME B16.5 Class 150.

Female threaded ISO 7 Rp (threaded flanges).

Others on request.

INSTALLATION: Horizontal installation in a closed loop system. An

example is shown in Fig. 1. See IMI - Installation

and maintenance instructions.

MOTIVE MEDIUM: Saturated steam.







CE MARKING – GROUP 2 (PED – European Directiv								
PN 16	Category							
All sizes	2 (CE marked)							



We reserve the right to change the design and material of this product without notice

IS 9.084 E 13.13

LRQA ISO 9001



LIMITING CONDITIONS										
Minimum density	0,80 kg/L									
Maximum motive pressure	10 bar									
Minimum motive pressure	1 bar									
Maximum operating temperature	185 °C									
Minimum operating temperature	0 °C									
Pump discharge per cycle (approx.)	22 L									

Remark: It is recommended that the motive pressure does not exceed 1 to 4 bar above the expected back pressure applied to the pump.

#### FLOW RATE CAPACITY (kg/h) OPERATING IN PUMP MODE W/ 300 mm FILLING HEAD

MOTIVE PRESSURE (bar)	TOTAL LIFT (bar)	2" x 2" DN 50 x 50	3" x 2" DN 80 x 50
1		2290	2640
2		3130	3610
3		3530	4070
4	0,35	3810	4390
6		3910	4500
8		3960	4570
10		3970	4580
2		2520	2910
3		2960	3420
4	_	3130	3610
6	1	3220	3710
8		3250	3750
10		3290	3800
3		2440	2810
4	2	2590	2990
5		2800	3220
6		2830	3270
8		2850	3290
10		2870	3300
4		2330	2680
5		2510	2900
6	3	2530	2920
8		2560	2960
10	1	2620	3030
5		2250	2600
6	4	2430	2810
8	1 4	2470	2860
10	1	2510	3010
6		2050	2370
8	5	2150	2490
10		2190	2540
7		1850	2140
8	6	1910	2210
10		2120	2450

BODY LIMITING CONDITIONS *										
APS	STS		APSTSS							
	IGED LASS 150	FLANGED PN 16	FLANGED CLASS 150	RELATED						
ALLOWABLE PRESSURE	RELATED TEMP.	ALLOWABLE PRESSURE	ALLOWABLE PRESSURE	TEMP.						
16 bar	50 °C	16 bar	15,3 bar	50 °C						
14 bar	100 °C	15 bar	13,3 bar	100 °C						
13 bar	195 °C	12,7 bar	11,1 bar	200 °C						
12 bar	250 °C	12 bar	10,2 bar	250 °C						

<sup>\*</sup> Rating according to EN 1092-1:2018.

#### RECEIVER SIZING TABLE FOR EQUALIZED, CLOSED SYSTEM INSTALLATION

			RECE	VER SIZ	E (DN)						
FLOW RATE (kg/h)	40	50	80	100	150	200	250				
(9,)	RECEIVER LENGTH (mm)										
≤ 300	1200	700	_	_	_	_	_				
400	1500	1000	_	-	_	_	_				
500	2000	1200	500	-	_	_	_				
600	_	1500	600	-	_	_	-				
800	_	2000	800	500	_	_	-				
1000	_	_	1000	700	_	_	-				
1500	_	_	1500	1000	_	_	_				
2000	_	_	2000	1300	600	_	_				
3000	-	_	_	2000	900	500	-				
4000	_	_	_	_	1200	700	_				
5000	_	_	_	-	1400	800	500				
6000	_	_	_	_	1700	1000	600				
7000	_	_	_	_	2000	1200	700				
8000	-	_	_	-	_	1300	800				
9000	_	_	_	_	_	1500	900				
10000	-	_	_	-	_	1700	1000				

Remark: Receiver length can be reduced by 50% when the motive inlet pressure divided by the backpressure is  $\geq 2$ .

#### **CAPACITY CORRECTION FACTORS FOR FILLING HEADS** OTHER THAN 300 mm

PUMP SIZE	FILLING HEAD "H" (mm)								
PUIVIP SIZE	150	300	600	900					
All sizes	0,7	1	1,2	1,35					

Remark: Filling head "H" is shown in Fig. 1.

## FLOW RATE CAPACITY (kg/h) OPERATING IN STEAM TRAP MODE

MODEL	SIZE		DIFFERENTIAL PRESSURE (bar)									
MODEL	SIZE	0,1	0,3	0,5	0,7	1	1,5	2	4,5	7	10	
APST	2" x 2" – DN 50 x 50	1800	3000	3900	4450	5000	6100	7100	10000	13750	16000	
APST-HC	2" x 2" – DN 50 x 50	2400	5900	7550	9050	11000	14000	15500	22500	26500	30000	
APST	3" x 2" – DN 80 x 50	1800	3000	3900	4450	5000	6100	7100	10000	13750	16000	
APST-HC	3" x 2" – DN 80 x 50	2400	5900	7550	9050	11000	14000	15500	22500	26500	30000	

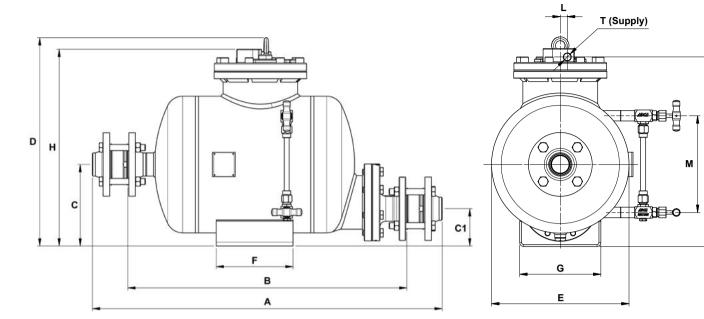
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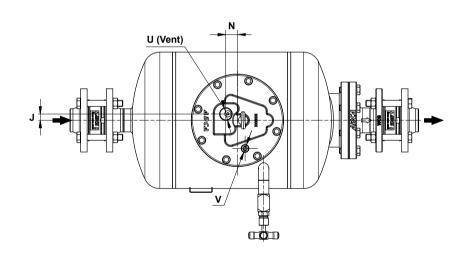
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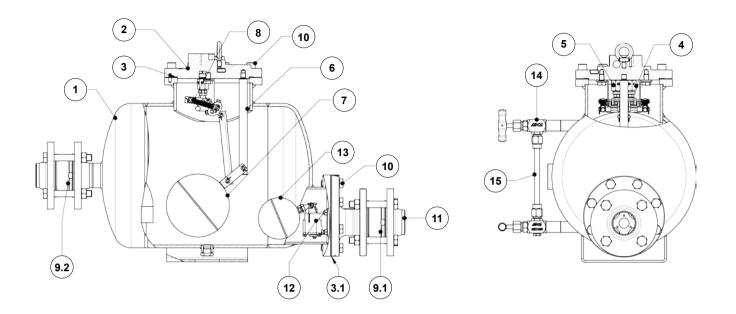
	DIMENSIONS (mm) – PN 16																		
SIZE	A*	B *	С	C1	D	E	F	G	Н	1	J	L	М	N	T **	U **	V **	WGT. (kg)	VOL. (L)
DN 50 x 50	910	726	212	97	542	356	200	210	512	490	17	18	250	30	1/2"	1"	1/2"	84	45
DN 80 x 50	924	728	212	97	542	356	200	210	512	490	17	18	250	30	1/2"	1"	1/2"	91	45

	DIMENSIONS (mm) – CLASS 150																		
SIZE	A *	B*	С	C1	D	E	F	G	Н	1	J	L	М	N	T **	U **	V **	WGT. (kg)	VOL. (L)
2" x 2"	958	743	212	97	542	356	200	210	512	490	16	18	250	30	1/2"	1"	1/2"	86	45
3" x 2"	980	748	212	97	542	356	200	210	512	490	16	18	250	30	1/2"	1"	1/2"	90	45

<sup>\*</sup> Dimensions are different if ISO 7 Rp female threaded flanges are requested.







MATERIALS									
POS. Nº	DESIGNATION	APSTS	APSTSS						
1	Body	P265GH / 1.0425 ; P235GH / 1.0345 ; S235JR / 1.0038	AISI 316 / 1.4401; AISI 316L / 1.4404						
2	Cover	GJS-400-15 / 0.7040	A351 CF8M / 1.4408						
3	* Cover gasket	Non asbestos	Non asbestos						
3.1	* Outlet cover gasket	Non asbestos	Non asbestos						
4	* Intake valve/seat assembly	Stainless steel	Stainless steel						
5	* Exhaust valve/seat assembly	Stainless steel	Stainless steel						
6	Pump mechanism	Stainless steel	Stainless steel						
7	*Float	Stainless steel	Stainless steel						
8	Spring assembly (2 pcs.)	Inconel	Inconel						
9.1	* Outlet check valve	A351 CF8M / 1.4408	A351 CF8M / 1.4408						
9.2	* Inlet check valve	A351 CF8M / 1.4408	A351 CF8M / 1.4408						
10	Bolts	Steel 8.8	Stainless steel A2-70						
11	Counter flanges	P250GH / 1.0460	AISI 316 / 1.4401						
12	* Steam trap mechanism	Stainless steel	Stainless steel						
13	* Steam trap float	Stainless steel	Stainless steel						
14	Level gauge cocks	Bronze / Stainless steel	Stainless steel						
15	Tube glass	Borosilicate	Borosilicate						

<sup>\*</sup> Available spare parts.

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<sup>\*\*</sup> As standard, in versions manufactured with EN 1092-1 PN 16 flanges, these connections are female threaded ISO 7 Rp. In versions with ASME B16.5 flanges, these connections are female threaded NPT.







To accurately size a pump trap, the following information must be provided:

- 1. Heat exchanger (or process equipment) maximum steam or condensate load, in kg/h.
- 2. Heat exchanger (or process equipment) operating pressure at full load in bar or, alternatively, the heat exchanger maximum operating pressure in bar and the over design percentage.
- 3. Motive steam pressure available to operate the pump trap, in bar.
- 4. The total lift or backpressure in bar the pump will have to overcome. This includes the change in fluid level elevation after the pump (0.0981 bar/m of lift), plus pressure in the return piping, plus the pressure drop caused by pipe friction and other system components.
- 5. Maximum controlled temperature of the medium to be heated (secondary fluid outlet temperature), in °C.
- 6. Minimum temperature of the medium to be heated (secondary fluid minimum inlet temperature), in °C.
- 7. Available filling head (H) in mm or any other dimension that allows its determination. See Fig. 1.

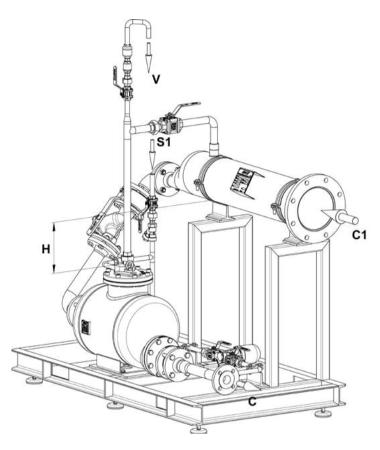
For information on how to predict stall refer to IS 9.085 Technical Information Sheet - Understanding stall condition - or consult the manufacturer.

## RECEIVER

A receiver is recommended to temporarily hold the liquid and prevent any flooding of the equipment, while the pump is performing a pumping cycle. A definable length of large diameter pipe can be used. See receiver sizing table.

NOTE: All ADCAMat automatic pump traps feature two mechanisms, combining the characteristics of a float steam trap and a pressure operated pump. When certain that the system backpressure is always superior to the equipment upstream pressure then an ADCAMat pressure operated pump (without steam trap) is the ideal solution as long as it is installed in a closed loop.

In extreme cases, where the system condensate load is above the discharge capacity of all ADCAMat automatic pump trap models, it is recommended to install an ADCAMat pressure operated pump in combination with a high capacity FLT series steam trap. In such scenarios, please consult the manufacturer.



H – Filling head S1 – Motive steam C1 – Condensate from heat process C – Condensate return V – Automatic air venting

Fig.1





### OPERATION



1. In the first instance, the steam intake valve is closed, while the vent valve is open. As condensate flows into the body through the inlet check valve, the APST can operate in a closed loop application, in one of two ways (as a steam trap or pressure operated pump).



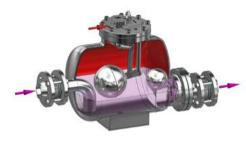
2. If the inlet pressure is greater than the back pressure, the APST works as a steam trap, continuously discharging condensate by differential pressure. At this point the steam intake valve remains closed and the vent valve open.



3. As soon as, e.g., the equipment control valve starts to modulate, the steam pressure will decrease. The lower differential pressure decreases the APST's ability to discharge as a steam trap, causing the condensate level to rise inside the body. Vacuum may even occur at this stage.



4. If this situation would persist, the condensate would eventually flood the equipment, causing problems. However, by using an APST, as the float reaches its highest position, the snap action mechanism actuates, closing the vent valve and opening the steam intake valve. Steam will then replace the necessary positive pressure to pump out the condensate. At this point the APST works as a pressure operated pump.



5. The float starts to fall as the condensate level inside the body drops and is discharged to the return system. When the float reaches its lowest position, the snap action mechanism resets.



6. As the motive steam valve closes and the vent valve opens, equalizing the body pressure with the upstream pressure, the condensate is allowed to flow once again into the APST. The cycle then repeats itself and, with enough differential pressure, the APST resumes as a steam trap or, otherwise, as a pump.

IS 9.084 E 13.13





# **AUTOMATIC PUMP TRAP PPT14**

#### DESCRIPTION

The ADCAMat PPT14 automatic pump trap is especially recommended where stall condition may occur due to poor steam trap condensate discharge capacity, caused by temporary insufficient pressure drop.

The equipment combines the features of a float steam trap and a pressure operated pump, in one single unit.

Whenever the steam trap function is incapable of draining condensate, the pump function is activated (using external steam pressure). The pump replaces the necessary positive pressure to lift the condensate to the return system, before water logging occurs, avoiding water hammer and consequent noise, equipment damage, corrosion, unstable temperature control, etc.

## MAIN FEATURES

Compact design.

Hardened stainless steel wear parts.

High-endurance inconel springs.

Low filling head to minimize installation space.

No electric requirements or NPSH issues.

Suitable for hazardous environments.

Low running costs.

No motive or flash steam is lost.

Operation under vacuum conditions.

**OPTIONS:** Level gauge.

USE: Drain and lift steam condensate from heat

exchangers, among others.

**AVAILABLE** 

MODELS: PPT14S – carbon steel.

PPT14SS - stainless steel.

SIZES: 11/2" x 1" and 2" x 11/2".

DN 40 x 25 and DN 50 x 40.

CONNECTIONS: Flanged EN 1092-1 PN 16.

Flanged ASME B16.5 Class 150.

Female threaded ISO 7 Rp (threaded flanges).

Others on request.

INSTALLATION: Horizontal installation in a closed loop system. An

example is shown in Fig. 1. See IMI – Installation

and maintenance instructions.

MOTIVE MEDIUM: Saturated steam.

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CE MARKING - GROUP 2 (	PED – European Directive)
PN 16	Category
All sizes	2 (CE marked)







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LIMITING CONDITIONS									
Liquid specific gravity	0,8 to 1								
Maximum motive inlet pressure	10 bar								
Minimum motive inlet pressure	1 bar								
Maximum operating temperature	185 °C								
Minimum operating temperature	0 ℃								
Pump discharge per cycle (approx.)	11 L								
D and a 14 to and a second and 4b a 4 4b a second to 12 t									

Remark: It is recommended that the motive inlet pressure does not exceed 1 to 4 bar above the expected pump backpressure.

### FLOW RATE CAPACITY (kg/h) OPERATING IN PUMP MODE W/ 300 mm FILLING HEAD

MOTIVE PRESSURE (bar)	TOTAL LIFT (bar)	11/2" x 1" DN 40 x 25	2" x 11/2" DN 50 x 40				
1		1050	1220				
2		1190	1490				
3		1220	1530				
4	0,35	1280	1600				
6		1310	1640				
8		1380	1730				
10		1460	1830				
2		940	1180				
3		1020	1280				
4	1	1110	1390				
6	'	1200	1510				
8		1290	1620				
10		1380	1730				
3		720	900				
4		850	1070				
5		940	1180				
6	2	1010	1260				
8		1130	1410				
10		1200	1490				
4		620	780				
5		730	920				
6	3	840	1050				
8		980	1230				
10		1090	1370				
5		540	680				
6	4	690	870				
8	4	880	1100				
10		960	1190				
6		520	650				
8	5	730	910				
10		840	1060				
7		530	670				
8	6	640	810				
10		730	920				

BODY LIMITING CONDITIONS *										
PPT14S PPT14SS										
FLAN PN 16 / C		FLANGED PN 16	FLANGED CLASS 150	RELATED						
ALLOWABLE PRESSURE	RELATED TEMP.	ALLOWABLE PRESSURE	ALLOWABLE PRESSURE	TEMP.						
16 bar	50 °C	16 bar	15,3 bar	50 °C						
14 bar	100 °C	15 bar	13,3 bar	100 °C						
13 bar	195 °C	12,7 bar	11,1 bar	200 °C						
12 bar	250 °C	12 bar	10,2 bar	250 °C						

<sup>\*</sup> Rating according to EN 1092-1:2018.

#### RECEIVER SIZING TABLE FOR EQUALIZED, CLOSED SYSTEM INSTALLATION

EI 014 D 4 E E			RECE	VER SIZ	E (DN)		
FLOW RATE (kg/h)	40	50	80	100	150	200	250
(3)			RECEIVE	R LENG	TH (mm)	)	
≤ 300	1200	700	_	_	_	_	_
400	1500	1000	_	_	_	_	_
500	2000	1200	500	_	_	_	_
600	-	1500	600	_	_	_	_
800	-	2000	800	500	_	_	_
1000	_	_	1000	700	_	_	_
1500	_	_	1500	1000	_	_	_
2000	-	_	2000	1300	600	_	_
3000	-	_	_	2000	900	500	_
4000	-	_	_	_	1200	700	_
5000	_	_	_	_	1400	800	500
6000	-	_	_	_	1700	1000	600
7000	_	_	_	_	2000	1200	700
8000	-	_	-	-	-	1300	800
9000	-	_	-	-	_	1500	900
10000	_	_	_	_	_	1700	1000

Remark: Receiver length can be reduced by 50% when the motive inlet pressure divided by the backpressure is  $\geq 2$ .

#### CAPACITY CORRECTION FACTORS FOR FILLING HEADS OTHER THAN 300 mm

PUMP SIZE		FILLING HEA		
PUIVIP SIZE	150	300	600	900
All sizes	0,7	1	1,2	1,35

Remark: Filling head (H) is shown in Fig. 1.

#### FLOW RATE CAPACITY (kg/h) OPERATING IN STEAM TRAP MODE

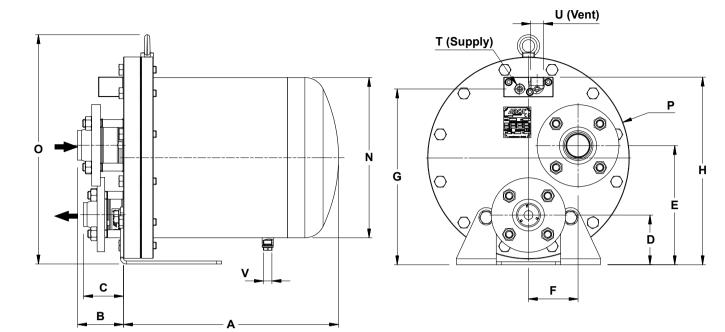
MODEL	SIZE	DIFFERENTIAL PRESSURE (bar)											
WIODEL	SIZE	0,1	0,3	0,5	0,7	1	1,5	2	3	4	5	7	10
PPT14	11/2" x 1" – DN 40 x 25	650	1100	1500	1700	2000	2600	3000	3510	3990	4400	5400	6200
PPT14	2" x 11/2" – DN 50 x 40	1050	1750	2400	2700	3400	3900	4500	5900	6600	7650	8500	10100

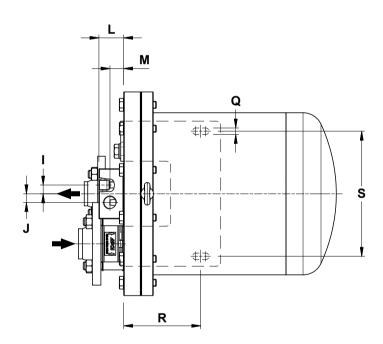
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									DIME	NSIO	NS (m	m) – F	PN 16										
SIZE	Α	В*	C *	D	E	F	G	н	ı	J	L	М	N	О	Р	Q	R	s	T **	U **	V **	WGT. (kg)	VOL. (L)
DN 40 x 25	425	80	64	100	240	100	354	378	17,5	17,5	50	28	324	464	407	13	154	250	1/2"	3/4"	3/8"	81,2	25
DN 50 x 40	425	91	79	100	240	100	354	378	17,5	17,5	50	28	324	464	407	13	154	250	1/2"	3/4"	3/8"	84	25

								DII	MENS	IONS	(mm)	– CL	ASS 1	50									
SIZE	Α	В*	C *	D	E	F	G	Н	ı	J	L	М	N	0	Р	Q	R	S	T **	U **	V **	WGT. (kg)	VOL. (L)
11/2" x 1"	425	97	80	100	240	100	354	378	17,5	17,5	50	28	324	464	407	13	154	250	1/2"	3/4"	3/8"	80,6	25
2" x 11/2"	425	106	96	100	240	100	354	378	17,5	17,5	50	28	324	464	407	13	154	250	1/2"	3/4"	3/8"	83,3	25

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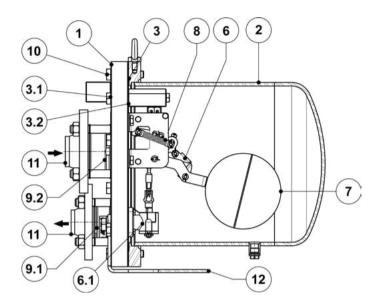
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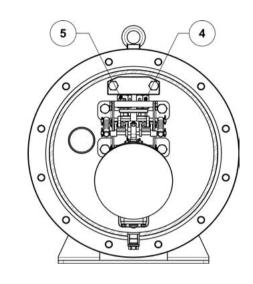




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	MATERIALS									
POS. Nº	DESIGNATION	PPT14S	PPT14SS							
1	Body	S355JR / 1.0045	AISI 316 / 1.4401; AISI 316L / 1.4404							
2	Cover	S355JR / 1.0045; P265GH / 1.0425; P235GH / 1.0345	AISI 304 / 1.4301; AISI 316 / 1.4401							
3	* Cover gasket	Stainless steel / Graphite	Stainless steel / Graphite							
3.1	* Gasket	Stainless steel / Graphite	Stainless steel / Graphite							
3.2	* Gasket	Stainless steel / Graphite	Stainless steel / Graphite							
4	* Intake valve/seat assembly	Stainless steel	Stainless steel							
5	* Exhaust valve/seat assembly	Stainless steel	Stainless steel							
6	Pump mechanism	Stainless steel	Stainless steel							
6.1	Steam trap mechanism	Stainless steel	Stainless steel							
7	* Float	Stainless steel	Stainless steel							
8	* Spring assembly (2 pcs.)	Inconel	Inconel							
9.1	* Outlet check valve	A351 CF8M / 1.4408	A351 CF8M / 1.4408							
9.2	* Inlet check valve	A351 CF8M / 1.4408	A351 CF8M / 1.4408							
10	Bolts	Steel 8.8	Stainless steel A2-70							
11	Counter flanges	P250GH / 1.0460	AISI 316 / 1.4401							
12	Supporting frame	S235JR / 1.0038	AISI 304 / 1.4301							

<sup>\*</sup> Available spare parts.

<sup>\*</sup> Dimensions are different if ISO 7 Rp female threaded flanges are requested.

\*\* As standard, in versions manufactured with EN 1092-1 PN 16 flanges, these connections are female threaded ISO 7 Rp. In versions with ASME B16.5 flanges, these connections are female threaded NPT.





## SIZING

To accurately size a pump trap, the following information must be provided:

- 1. Heat exchanger (or process equipment) maximum steam or condensate load, in kg/h.
- 2. Heat exchanger (or process equipment) operating pressure at full load in bar or, alternatively, the heat exchanger maximum operating pressure in bar and the over design percentage.
- 3. Motive steam pressure available to operate the pump trap, in bar.
- 4. The total lift or backpressure in bar the pump will have to overcome. This includes the change in fluid level elevation after the pump (0.0981 bar/m of lift), plus pressure in the return piping, plus the pressure drop caused by pipe friction and other system components.
- 5. Maximum controlled temperature of the medium to be heated (secondary fluid outlet temperature), in °C.
- 6. Minimum temperature of the medium to be heated (secondary fluid minimum inlet temperature), in °C.
- 7. Available filling head (H) in mm or any other dimension that allows its determination. See Fig. 1.

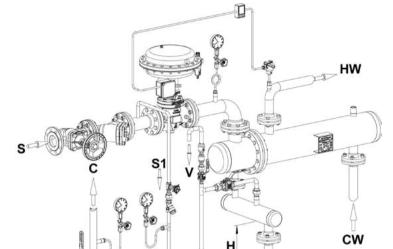
For information on how to predict stall refer to IS 9.085 Technical Information Sheet - Understanding stall condition - or consult the manufacturer.

## RECEIVER

A receiver is recommended to temporarily hold the liquid and prevent any flooding of the equipment, while the pump is performing a pumping cycle. A definable length of large diameter pipe can be used. See receiver sizing table.

NOTE: All ADCAMat automatic pump traps feature two mechanisms, combining the characteristics of a float steam trap and a pressure operated pump. When certain that the system backpressure is always superior to the equipment upstream pressure then an ADCAMat pressure operated pump (without steam trap) is the ideal solution as long as it is installed in a closed loop.

In extreme cases, where the system condensate load is above the discharge capacity of all ADCAMat automatic pump trap models, it is recommended to install an ADCAMat pressure operated pump in combination with a high capacity FLT series steam trap. In such scenarios, please consult the manufacturer.



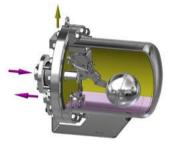
H – Filling head
S – Process steam supply
S1 – Motive steam
C – Condensate return
V – Automatic air venting
CW – Cold water inlet
HW – Hot water outlet

Fig.1

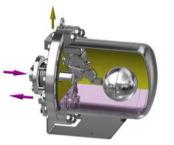




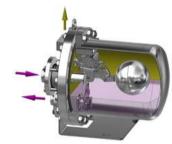
## OPERATION



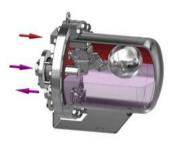
1. In the first instance, the steam intake valve is closed, while the vent valve is open. As condensate flows into the body through the inlet check valve, the PPT14 can operate in a closed loop application, in one of two ways (as a steam trap or pressure operated pump).



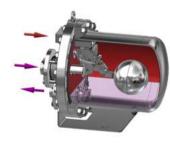
2. If the inlet pressure is greater than the back pressure, the PPT14 works as a steam trap, continuously discharging condensate by differential pressure. At this point the steam intake valve remains closed and the vent valve open.



3. As soon as, e.g., the equipment control valve starts to modulate, the steam pressure will decrease. The lower differential pressure decreases the PPT14's ability to discharge as a steam trap causing the condensate level to rise inside the body. Vacuum may even occur at this stage.



4. If this situation would persist, the condensate would eventually flood the equipment, causing problems. However, by using a PPT14, as the float reaches its highest position, the snap action mechanism actuates, closing the vent valve and opening the steam intake valve. Steam will then replace the necessary positive pressure to pump out the condensate. At this point the PPT14 works as a pressure operated pump.



5. The float starts to fall as the condensate level inside the body drops and is discharged to the return system. When the float reaches its lowest position, the snap action mechanism resets.



6. As the motive steam valve closes and the vent valve opens, equalizing the body pressure with the upstream pressure, the condensate is allowed to flow once again into the PPT14. The cycle then repeats itself and, with enough differential pressure, the PPT14 resumes as a steam trap or, otherwise, as a pump.

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